

A large, stylized illustration of an industrial facility, likely a medical device manufacturing plant, rendered in a dark blue silhouette against a lighter blue background. The facility includes several tall smokestacks, various buildings, and a complex network of pipes and structural elements. From the smokestacks, thick, wavy plumes of smoke or steam rise into the sky, filling the upper right portion of the image. The entire scene is set against a gradient background that transitions from a light blue at the top to a darker blue at the bottom.

## Source Test Report

Becton-Dickinson Medical  
920 East 19<sup>th</sup> Street  
Columbus, Nebraska 68601

Catalytic Oxidizer -  
Ethylene Oxide DRE Test

Test Date: July 11, 2018

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AST Project No. 2018-0668D



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### Regulatory Information

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*Permit No.(s)*  
*Regulatory Citation(s)* 40 CFR Part 63, Subpart O

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### Source Information

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*Source Name*  
Sterilization Chamber –  
Catalytic Oxidizer

*Target Parameter(s)*  
Ethylene Oxide - DRE

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### Contact Information

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*Test Location*  
BD Medical  
920 East 19<sup>th</sup> Street  
Columbus, Nebraska 68601

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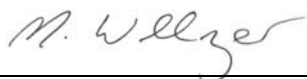
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Alliance Source Testing, LLC (AST) has completed the source testing as described in this report. Results apply only to the source tested and operating conditions for the specific test date and time(s) identified within this report. All results are intended to be considered in their entirety, and AST is not responsible for use of less than the complete test report without written consent. This report shall not be reproduced in full or in part without written approval from the customer.

To the best of my knowledge and abilities, all information, facts and test data are correct. Data presented in this report have been checked for completeness and are accurate, error-free and legible. Onsite testing was conducted in accordance with approved procedures. Any deviations or problems are detailed in the relevant sections on the test report.

This report is only considered valid once an authorized representative of AST has signed in the space provided below; any other version is considered draft. This document was prepared in portable document format (.pdf) and contains pages as identified in the bottom footer of this document.



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July 26, 2018

Date



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## TABLE OF CONTENTS

1.0	Introduction .....	1-1
1.1	Facility Description/ Source and Control System Descriptions .....	1-1
1.2	Site Specific Test Plan/Test Protocol & Notification.....	1-1
1.3	Test Program Notes.....	1-1
2.0	Summary of Results .....	2-1
3.0	Testing Methodology.....	3-1
3.1	U.S. EPA Reference Test Methods 1 and 2 – Volumetric Flow Rate.....	3-1
3.2	U.S. EPA Reference Test Method 4 – Gas Moisture Content.....	3-1
3.3	U.S. EPA Reference Test Method 18 – Ethylene Oxide .....	3-2

## LIST OF TABLES

Table 1-1	Emission Limits .....	1-1
Table 2-1	Summary of Results.....	2-2

## APPENDICES

Appendix A	.....	Sample Calculations
Appendix B	.....	Field Data
Appendix C	.....	Quality Assurance/Quality Control Data
Appendix D	.....	Process Operating/Control System Data

Introduction

## 1.0 Introduction

Alliance Source Testing, LLC (AST) was retained by Becton-Dickinson Medical (BD Medical) to conduct compliance testing on the ethylene oxide (EO) sterilization chamber at the BD Medical facility located in Columbus, Nebraska. Performance tests were conducted to quantify the concentrations and mass rates of EO into and out of the catalytic oxidizer to determine the EO destruction removal efficiency (DRE) on a mass basis. The performance test was conducted to satisfy testing requirements and demonstrate compliance with emission standards outlined in 40 CFR Part 63, Subpart O – Ethylene Oxide Emissions Standards for Sterilization Facilities. The catalytic oxidizer is required to demonstrate 99% DRE of EO.

## 1.1 Facility Description/ Source and Control System Descriptions

An EO sterilization chamber is in service at the BD Medical facility in Columbus, Nebraska. A catalytic oxidizer is used for control of EO emissions. The source identification and operating standards are provided in Table 1-1.

**Table 1-1**  
**Emission Limits**

Source	Pollutant	Citation
Catalytic Oxidizer	Ethylene Oxide DRE $\geq$ 99% Catalyst bed outlet temperature to be recorded	40 CFR Part 63, Subpart O

## 1.2 Test Protocol & Notification

Testing was conducted in accordance with the test protocol submitted to NDEQ by BD Medical.

## 1.3 Test Program Notes

No test method deviations occurred during testing, except as noted in the test protocol.

At the inlet sampling location, AST did not conduct EPA Method 4 sampling for measuring moisture content, due to the possible EO exposure risks. Moisture content was measured from the outlet sampling location and used for both the inlet and outlet volumetric flow calculations and converting EO concentrations to a dry basis. EPA Method 4 sampling was completed from a single sample point at the outlet sampling location.

EO was not detected at the outlet. An onsite reporting limit of 0.14 parts per million, wet volume basis (ppmvw) was reported for outlet test runs. EO levels detected at outlet were closer to 0.05 ppmvw.

## Summary of Results

## 2.0 Summary of Results

AST conducted compliance testing on the EO sterilization chamber on July 11, 2018.

Three (3), 1-hour test runs will be conducted to determine the concentrations of EO into and out of the sterilization chamber. Concurrent volumetric flow rate (VFR) measurements were conducted to calculate mass rates. Since the contents of the gas streams are essentially air, a dry molecular weight of 29.0 was assumed for gas velocity calculations. EO DRE was determined by comparing the inlet and outlet EO levels on a mass basis.

Testing involved direct-interface EPA Method 18 on-site gas chromatographs equipped with flame ionization detectors (GCFID) to determine the inlet and outlet levels of EO. The GCFID were calibrated with EO balanced nitrogen standards certified to 2% accuracy and dilutions of certified standards. Due to the presence of methane in the exhaust, a sample of exhaust gas was collected in a Tedlar bag and spiked with a known concentration (50 ppm) of EO to demonstrate adequate EO quantification and recovery.

The involved processes were operating under normal conditions. Applicable operating and control equipment parameters were recorded throughout the test program by BD Medical personnel for inclusion in the test report, including;

- Catalyst bed outlet temperature

Table 2-1 provide a summary of the emission testing results with comparisons to the applicable limits. Any difference between the summary results listed in the following table and the detailed results contained in appendices are due to rounding for presentation.



**Table 2-1**  
**Summary of Results**

Emissions Data					
Run Number	1	2	3	Average	Emission
Date	07/11	07/11	07/11	--	Standard
<b>Operating Data</b>					
Catalyst Bed Outlet Temperature, °C	169.3	185.0	193.1	182.5	
<b>Inlet Data</b>					
H <sub>2</sub> O Concentration, %vd	3.4	3.1	2.7	3.1	
VFR, dscfm	4,394	4,216	4,228	4,279	
EO Concentration, ppmvd	680.1	956.9	1,129.1	922.0	
EO Rate, lb/hr	20.48	27.65	32.72	26.95	
<b>Outlet Data</b>					
H <sub>2</sub> O Concentration, %vd	3.4	3.1	2.7	3.1	
VFR, dscfm	4,947	4,257	4,255	4,486	
EO Concentration, ppmvd	0.15	0.15	0.15	0.15	
EO Rate, lb/hr	0.005	0.004	0.004	0.005	
<b>DRE Data</b>					
EO DRE (lb/hr), %	99.98	99.98	99.99	99.98	99

## Testing Methodology

### 3.0 Testing Methodology

Testing was conducted in accordance with U.S. Environmental Protection Agency (EPA) Reference Test Methods (RM) 1, 2, 4 and 18 referenced in 40 CFR Part 60, Appendix A. The emission testing program was conducted in accordance with the test methods listed in Table 3-1. Method descriptions are provided below while quality assurance/quality control (QA/QC) data are provided in Appendix C.

**Table 3-1**  
**Source Testing Methodology**

Parameter	U.S. EPA Reference Test Methods	Notes
VFR	1-2	Full Velocity Traverses
O <sub>2</sub> , CO <sub>2</sub>	2	Assumed Ambient
H <sub>2</sub> O	4	Gravimetric Analysis
EO	18	Gas Chromatograph

#### 3.1 U.S. EPA Reference Test Methods 1 and 2 – Volumetric Flow Rate

The sampling location and number of traverse points were selected in accordance with EPA RM 1. To determine the minimum number of traverse points, the upstream and downstream distances were equated into equivalent diameters and compared to Figure 1-2 in EPA RM 1. All stack diameters, depths, widths, upstream and downstream disturbance distances and nipple lengths were measured on site with a verification measurement provided by the Field Team Leader.

Full velocity traverses were conducted in accordance with EPA RM 2 to determine the stack gas velocity pressure, static pressure and temperature. The velocity and static pressure measurement system consisted of a pitot tube and inclined manometer. The stack gas temperature was measured with a K-type thermocouple and pyrometer. The pitot assembly was leak checked pre and post each sampling period.

The temperature and differential pressure traverse data were combined with concurrently collected diluent data to calculate the stack gas velocity and volumetric flow rate in units of feet per second (ft/sec), actual cubic feet per minute (acfm), dry standard (1 atmosphere and 68°F) cubic feet per minute (dscfm) and pounds per hour (lb/hr). Since the contents of the gas streams are essentially air, a dry molecular weight of 29.0 was assumed for gas velocity calculations.

#### 3.2 U.S. EPA Reference Test Method 4 – Moisture Content

The stack gas moisture content was determined in accordance with EPA RM 4.

For each test run, a sample of gas for moisture determination was extracted from the stack at a constant flow rate of no more than 0.75 cubic feet per minute (cfm). The gas sample was passed through a stainless-steel probe, through a series of four (4) chilled glass impingers, and through a calibrated dry gas meter. In lieu of EPA RM 4 Section 8.1.1.1 requirements, a single sample point was used for moisture determination.

Prior to sampling, the first two impingers each were seeded with 100 milliliters of water. The third impinger was empty. The fourth impinger was seeded with 250 grams of dried silica gel. The sampling system was leak checked

pre and post each sampling period. Following sampling, the moisture gain in the impingers was measured gravimetrically and compared to the total sample volume (standard conditions) to determine the moisture content of the gas. The measured moisture content was compared to the saturation moisture content at stack temperature and pressure. The lower of the two moisture content values was reported.

### 3.3 U.S. EPA Reference Test Method 18 – Ethylene Oxide

Ethylene oxide concentrations were measured in accordance with EPA RM 18 using the direct interface sampling and analysis procedures detailed in the method. Samples were analyzed on-site with an HP Model 5890 Series II Gas Chromatograph equipped with dual RTX-1 columns to separate methane and EO, dual flame ionization detectors (FID) and Chemstation software.

Gas phase calibration standards were prepared by dilution of +/-2% accuracy certified gas standards. Preparation of diluted standards were conducted using a gas-tight volumetric syringe and new Tedlar bags. Triplicate injections were conducted for each standard, and a calibration curve of peak area versus concentration was prepared. A least squares line ( $y=mx$ ) was fit to the inlet and outlet data set.

Following the GC calibrations, a recovery study (line loss) was conducted using certified EO gas standards with approximate concentrations of 5000 ppm and 50 ppm of EO for the inlet and outlet sampling systems, respectively. A successful recovery study was demonstrated with the mean, triplicate GC response within 10% of the certified gas concentration.

Due to the presence of methane in the exhaust, prior to the test runs as well as during Run 2, a sample of exhaust gas was collected in a Tedlar bag. The contents of EO in the bag was quantified. Then the bag was spiked with a known concentration of EO to demonstrate adequate EO quantification and recovery. EO levels in the exhaust were below the reporting limit of 0.14 ppmvw.

EO levels were measured at the inlet and outlet simultaneously. A gas sample was transported directly to the GC gas sampling valves using a heated sample line. Samples were analyzed approximately once every 10-minutes. A “test run” consisted of five (5) consecutive injections. Three (3), test runs were conducted (for a total of 15 injections) at the inlet and outlet of the catalytic oxidizer.

After completing the 3 test runs, the mid-level calibration standards were re-analyzed at the gas sampling valve in triplicate. The average of the initial calibration response (triplicate average) and the post-test check response (triplicate average) were within 5% of their mean value, and the initial calibration linear regression data were used to quantify EO levels.

The results of the GC analyses were used to calculate EO levels in units of ppmvw. The data were combined with stack gas VFR and H<sub>2</sub>O data to calculate EO mass rates in units of pounds per hour (lb/hr) and concentrations in parts per million, dry volume basis (ppmvd). The catalytic oxidizer DRE will be calculated on a mass basis.

## Appendix A



Location Becton-Dickinson Medical  
 Source Catalytic Oxidizer - Outlet  
 Project No. 18-0668D  
 Run No. 1  
 Method VFR

Meter Pressure (Pm), in. Hg

$$Pm = Pb + \frac{\Delta H}{13.6}$$

where,

Pb	<u>28.44</u>	= barometric pressure, in. Hg
ΔH	<u>1.000</u>	= pressure differential of orifice, in H <sub>2</sub> O
Pm	<u>28.51</u>	= in. Hg

Absolute Stack Gas Pressure (Ps), in. Hg

$$Ps = Pb + \frac{Pg}{13.6}$$

where,

Pb	<u>28.44</u>	= barometric pressure, in. Hg
Pg	<u>-0.25</u>	= static pressure, in. H <sub>2</sub> O
Ps	<u>28.42</u>	= in. Hg

Standard Meter Volume (Vmstd), dscf

$$Vmstd = \frac{17.647 \times Y \times Vm \times Pm}{Tm}$$

where,

Y	<u>1.018</u>	= meter correction factor
Vm	<u>36.820</u>	= meter volume, cf
Pm	<u>28.51</u>	= absolute meter pressure, in. Hg
Tm	<u>551.0</u>	= absolute meter temperature, °R
Vmstd	<u>34.230</u>	= dscf

Standard Wet Volume (Vwstd), scf

$$Vwstd = 0.04707 \times Vlc$$

where,

Vlc	<u>25.9</u>	= volume of H <sub>2</sub> O collected, ml
Vwstd	<u>1.219</u>	= scf

Moisture Fraction (BWSsat), dimensionless (theoretical at saturated conditions)

$$BWSsat = \frac{10^{6.37 - \left(\frac{2,827}{Ts + 365}\right)}}{Ps}$$

where,

Ts	<u>163.3</u>	= stack temperature, °F
Ps	<u>28.42</u>	= absolute stack gas pressure, in. Hg
BWSsat	<u>0.367</u>	= dimensionless

Moisture Fraction (BWSmsd), dimensionless (measured)

$$BWS = \frac{Vwstd}{(Vwstd + Vmstd)}$$

where,

Vwstd	<u>1.219</u>	= standard wet volume, scf
Vmstd	<u>34.230</u>	= standard meter volume, dscf
BWS	<u>0.034</u>	= dimensionless

Moisture Fraction (BWS), dimensionless

$$BWS = BWSmsd \text{ unless } BWSsat < BWSmsd$$

where,

BWSsat	<u>0.367</u>	= moisture fraction (theoretical at saturated conditions)
BWSmsd	<u>0.034</u>	= moisture fraction (measured)
BWS	<u>0.034</u>	= dimensionless

Molecular Weight (WET) (Ms), lb/lb-mole

$$Ms = Md (1 - BWS) + 18 (BWS)$$

where,

Md	<u>29.00</u>	= molecular weight (DRY), lb/lb mol
BWS	<u>0.034</u>	= moisture fraction, dimensionless
Ms	<u>28.62</u>	= lb/lb mol



Location	Becton-Dickinson Medical
Source	Catalytic Oxidizer - Outlet
Project No.	18-0668D
Run No.	1
Method	VFR

Average Velocity (Vs), ft/sec

$$V_s = 85.49 \times C_p \times (\Delta P^{1/2})_{avg} \times \sqrt{\frac{T_s}{P_s \times M_s}}$$

where,

$C_p$	0.83	= pitot tube coefficient
$\Delta P^{1/2}$	0.565	= velocity head of stack gas, (in. H <sub>2</sub> O) <sup>1/2</sup>
$T_s$	623.3	= absolute stack temperature, °R
$P_s$	28.42	= absolute stack gas pressure, in. Hg
$M_s$	28.62	= molecular weight of stack gas, lb/lb mol
$V_s$	35.2	= ft/sec

Average Stack Gas Flow at Stack Conditions (Qa), acfm

$$Q_a = 60 \times V_s \times A_s$$

where,

$V_s$	35.2	= stack gas velocity, ft/sec
$A_s$	3.01	= cross-sectional area of stack, ft <sup>2</sup>
$Q_a$	6,366	= acfm

Average Stack Gas Flow at Standard Conditions (Qsw), scfm

$$Q_{sw} = 17.647 \times Q_a \times \frac{P_s}{T_s}$$

where,

$Q_a$	6,366	= average stack gas flow at stack conditions, acfm
$P_s$	28.42	= absolute stack gas pressure, in. Hg
$T_s$	623.3	= absolute stack temperature, °R
$Q_{sw}$	5,123	= scfm

Average Stack Gas Flow at Standard Conditions (Qsd), dscfm

$$Q_{sd} = 17.647 \times Q_a \times (1 - BWS) \times \frac{P_s}{T_s}$$

where,

$Q_a$	6,366	= average stack gas flow at stack conditions, acfm
$BWS$	0.034	= moisture fraction
$P_s$	28.42	= absolute stack gas pressure, in. Hg
$T_s$	623.3	= absolute stack temperature, °R
$Q_{sd}$	4,947	= dscfm

Dry Gas Meter Calibration Check (Yqa), dimensionless

$$Y_{qa} = \frac{Y - \left( \frac{\Theta}{V_m} \sqrt{\frac{0.0319 \times T_m \times 29}{\Delta H @ \times \left( P_b + \frac{\Delta H_{avg}}{13.6} \right) \times M_d}} \sqrt{\Delta H_{avg}} \right)}{Y} \times 100$$

where,

$Y$	1.018	= meter correction factor, dimensionless
$\Theta$	60	= run time, min.
$V_m$	36,820	= total meter volume, dcf
$T_m$	551.0	= absolute meter temperature, °R
$\Delta H @$	1.63	= orifice meter calibration coefficient, in. H <sub>2</sub> O
$P_b$	28.44	= barometric pressure, in. Hg
$\Delta H_{avg}$	1.000	= average pressure differential of orifice, in. H <sub>2</sub> O
$M_d$	29.00	= molecular weight (DRY), lb/lb mol
$(\Delta H)^{1/2}$	1.000	= average squareroot pressure differential of orifice, (in. H <sub>2</sub> O) <sup>1/2</sup>
$Y_{qa}$	1.6	= dimensionless

**Location:** Columbus Sterilization Plant  
**Source:** Catalytic Oxidizer  
**Project No.:** --  
**Run 1** Run 1

**Ethylene Oxide Mass Rate (ER<sub>CO</sub>), lb/hr**

$$ER_{CO} = \frac{C_{CO} \times MW \times Q_s \times 60 \times 28.32}{24.04 \times 1.0 E + 06 \times 454}$$

where,

$C_{CO}$  680.1 = EO concentration, ppmvd  
 MW 44.05 = EO molecular weight, g/g-mole  
 Qs 4,394 = stack gas volumetric flow rate at standard conditions, dscfm  
 ER<sub>CO</sub> 20.48 = lb/hr

**Ethylene Oxide Destruction Removal Efficiency (RE<sub>CO</sub>), %**

$$RE_{CO} = \left( \frac{C_{COe15I} - C_{COe15}}{C_{COe15I}} \right) \times 100$$

where,

$C_{COe15I}$  20.48 = EO Inlet Mass Rate, lb/hr  
 $C_{COe15}$  0.005 = EO Outlet Mass Rate, lb/hr  
 RE 99.98 = %



## Appendix B

Becton-Dickinson Medical  
Columbus, Nebraska  
Catalytic Oxidizer  
7/11/2018

Field Reference Method Data (Inlet)					
Run #	1	2	3	Average	
Start Time	10:00	11:10	12:20		
Stop Time	11:00	12:10	13:20		
Sample Time	60	60	60		
Method 18 GC Data (Inlet)					
<u>MW</u>	Run #	1	2	3	Average
44.05	Ethylene Oxide (ppmvw)	656.68	923.96	1090.30	890.31

Field Reference Method Data (Outlet)			
1	2	3	Average
10:00	11:10	12:20	
11:00	12:10	13:20	
60	60	60	
Method 18 GC Data (Outlet)			
1	2	3	Average
0.14	0.14	0.14	0.14

Reference Method Calculations (Inlet)					
Run #		1	2	3	Average
B <sub>ws</sub>	Moisture Content (%/100)	0.034	0.031	0.027	0.031
F <sub>DSCFM</sub>	Gas Flow (dscfm)	4,394	4,216	4,228	4,279
ppmvd	Ethylene Oxide (ppmvd)	680.1	956.9	1,129.1	922.0
lb/hr	Ethylene Oxide (lb/hr)	20.48	27.65	32.72	26.95
tpy	Ethylene Oxide (tpy)	89.7	121.1	143.3	118.04
DRE	DRE Ethylene Oxide - lb/hr (%)	99.98	99.98	99.99	99.98

Reference Method Calculations (Outlet)			
1	2	3	Average
0.034	0.031	0.027	0.031
4,947	4,257	4,255	4,486
0.15	0.15	0.15	0.15
0.005	0.004	0.004	0.005
0.02	0.02	0.02	0.02

Location Becton-Dickinson Medical

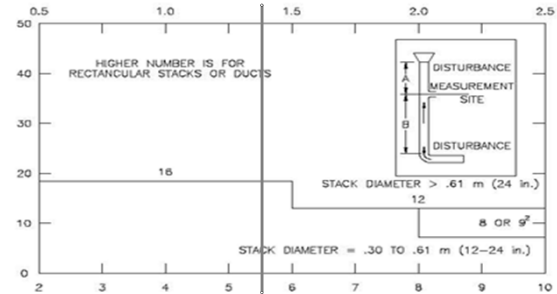
Source Catalytic Oxidizer - Outlet

Project No. 18-0668D

Date: 07/11/18

## Stack Parameters

Duct Orientation: Vertical  
Duct Design: Circular  
Distance from Far Wall to Outside of Port: 27.50 in  
Nipple Length: 4.25 in  
Depth of Duct: 23.50 in  
Width of Duct: -- in  
Cross Sectional Area of Duct: 3.01 ft<sup>2</sup>  
Equivalent Diameter: -- in  
No. of Test Ports: 2  
Distance A: 40.0 ft  
Distance A Duct Diameters: 20.4 (must be > 0.5)  
Distance B: 10.8 ft  
Distance B Duct Diameters: 5.5 (must be > 2)  
Minimum Number of Traverse Points: 16  
Actual Number of Traverse Points: 16



## CIRCULAR DUCT

### LOCATION OF TRAVERSE POINTS

Number of traverse points on a diameter

	2	3	4	5	6	7	8	9	10	11	12
1	14.6	--	6.7	--	4.4	--	3.2	--	2.6	--	2.1
2	85.4	--	25.0	--	14.6	--	10.5	--	8.2	--	6.7
3	--	--	75.0	--	29.6	--	19.4	--	14.6	--	11.8
4	--	--	93.3	--	70.4	--	32.3	--	22.6	--	17.7
5	--	--	--	--	85.4	--	67.7	--	34.2	--	25.0
6	--	--	--	--	95.6	--	80.6	--	65.8	--	35.6
7	--	--	--	--	--	--	89.5	--	77.4	--	64.4
8	--	--	--	--	--	--	96.8	--	85.4	--	75.0
9	--	--	--	--	--	--	--	--	91.8	--	82.3
10	--	--	--	--	--	--	--	--	97.4	--	88.2
11	--	--	--	--	--	--	--	--	--	--	93.3
12	--	--	--	--	--	--	--	--	--	--	97.9

\*Percent of stack diameter from inside wall to traverse point.

Traverse Point	% of Diameter	Distance from inside wall	Distance from outside of port
1	3.2	0.75	5.00
2	10.5	2.47	6.72
3	19.4	4.56	8.81
4	32.3	7.59	11.84
5	67.7	15.91	20.16
6	80.6	18.94	23.19
7	89.5	21.03	25.28
8	96.8	22.75	27.00
9	--	--	--
10	--	--	--
11	--	--	--
12	--	--	--

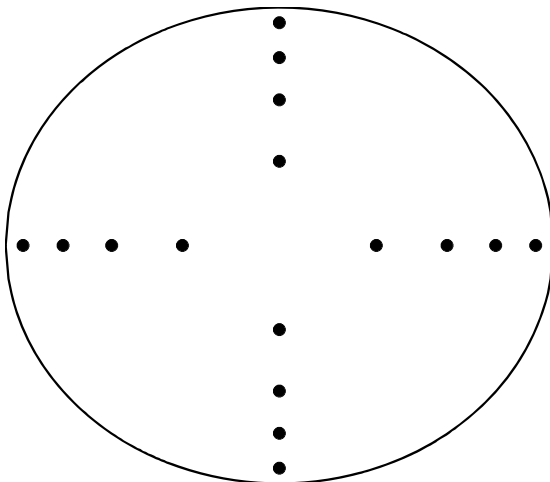
Stack Diagram

A = 40 ft.

B = 10.8 ft.

Depth of Duct = 23.5 in.

Cross Sectional Area



Downstream Disturbance

A

B

Upstream Disturbance

**Location** Becton-Dickinson Medical

**Source** Catalytic Oxidizer - Outlet

**Project No.** 18-0668D

**Date** 7/11/18

Sample Point	Angle ( $\Delta P=0$ )
1	4
2	3
3	6
4	6
5	9
6	7
7	12
8	10
9	7
10	5
11	8
12	6
13	8
14	9
15	10
16	13
Average	7.7

Location Becton-Dickinson Medical

Source Catalytic Oxidizer - Outlet

Project No. 18-0668D

Run No.	1		2		3	
Date	7/11/18		7/11/18		7/11/18	
Status	VALID		VALID		VALID	
Start Time	10:05		10:21		12:32	
Stop Time	10:15		10:34		12:41	
Leak Check	Pass		Pass		Pass	
Traverse Point	$\Delta P$ (in. WC)	Ts (°F)	$\Delta P$ (in. WC)	Ts (°F)	$\Delta P$ (in. WC)	Ts (°F)
A1	0.22	161	0.20	176	0.21	183
2	0.27	164	0.23	177	0.22	182
3	0.28	165	0.26	178	0.24	183
4	0.31	165	0.27	180	0.26	183
5	0.36	166	0.25	184	0.24	184
6	0.39	165	0.24	184	0.26	184
7	0.36	163	0.25	184	0.25	183
8	0.35	164	0.28	184	0.25	183
B1	0.24	164	0.18	172	0.21	182
2	0.29	164	0.23	178	0.23	183
3	0.32	165	0.25	181	0.25	183
4	0.33	163	0.26	180	0.26	182
5	0.35	162	0.23	180	0.23	183
6	0.36	160	0.24	178	0.25	184
7	0.36	161	0.24	179	0.25	185
8	0.35	160	0.26	179	0.25	185

Average					
Square Root of $\Delta P$ , (in. WC) <sup>1/2</sup>	( $\Delta P$ ) <sup>1/2</sup>	0.565	0.491	0.491	0.516
Average $\Delta P$ , in. WC	( $\Delta P$ )	0.32	0.24	0.24	0.27
Pitot Tube Coefficient	(Cp)	0.833	0.833	0.833	0.833
Barometric Pressure, in. Hg	(Pb)	28.44	28.44	28.44	28.44
Static Pressure, in. WC	(Pg)	-0.25	-0.24	-0.23	-0.24
Stack Pressure, in. Hg	(Ps)	28.42	28.42	28.42	28.42
Average Temperature, °F	(Ts)	163.3	179.6	183.3	175.4
Average Temperature, °R	(Ts)	623.3	639.6	643.3	635.4
Moisture Fraction	(BWS)	0.034	0.031	0.027	0.031
Molecular Weight, lb/lb-mole (dry)	(Md)	29.00	29.00	29.00	29.00
Molecular Weight, lb/lb-mole (wet)	(Ms)	28.62	28.66	28.70	28.66
Velocity, ft/sec	(Vs)	35.2	31.0	31.0	32.4
VFR at stack conditions, acfm	(Qa)	6,366	5,601	5,610	5,859
VFR at standard conditions, scfh	(Qsw)	307,404	263,533	262,478	277,805
VFR at standard conditions, scfm	(Qsw)	5,123	4,392	4,375	4,630
VFR at standard conditions, dscfm	(Qsd)	4,947	4,257	4,255	4,486

Location Becton-Dickinson Medical  
Source Catalytic Oxidizer - Outlet  
Project No. 18-0668D

Run No.	1	2	3
Date	7/11/18	7/11/18	7/11/18
Status	VALID	VALID	VALID
Start Time	10:00	11:10	12:20
End Time	11:00	12:10	13:20
Run Time, min (0)	60	60	60
Meter ID	M5-10	M5-10	M5-10
Meter Correction Factor (Y)	1.018	1.018	1.018
Orifice Calibration Value (ΔH @)	1.630	1.630	1.630
Max Vacuum, in. Hg	4.0	4.0	4.0
Post Leak Check, cfm (at max vac.)	PASS	PASS	PASS
Meter Volume, ft <sup>3</sup>			
Time	516.458		
0	516.458	553.372	591.000
5	519.500	556.500	594.100
10	522.500	559.600	597.200
15	525.500	562.600	600.300
20	528.600	565.700	603.400
25	531.700	568.800	606.560
30	534.760	572.000	609.800
35	537.800	575.000	612.800
40	540.800	578.100	615.900
45	543.900	581.200	619.000
50	547.000	584.400	622.100
55	550.100	587.500	625.200
60	553.278	590.745	628.407
Total Meter Volume, ft <sup>3</sup> (Vm)	36.820	37.373	37.407
Temperature, °F			
Time	Meter Imp. Exit	Meter Imp. Exit	Meter Imp. Exit
0	86.0 / 32.0	96.0 / 42.0	101.0 / 46.0
5	85.0 / 40.0	97.0 / 50.0	103.0 / 50.0
10	86.0 / 55.0	98.0 / 54.0	103.0 / 51.0
15	87.0 / 58.0	99.0 / 54.0	104.0 / 52.0
20	88.0 / 58.0	100.0 / 55.0	104.0 / 52.0
25	89.0 / 59.0	100.0 / 55.0	104.0 / 52.0
30	90.0 / 59.0	101.0 / 56.0	105.0 / 51.0
35	93.0 / 57.0	101.0 / 55.0	105.0 / 50.0
40	94.0 / 60.0	102.0 / 57.0	106.0 / 48.0
45	95.0 / 61.0	102.0 / 57.0	105.0 / 47.0
50	96.0 / 60.0	103.0 / 58.0	106.0 / 48.0
55	97.0 / 61.0	103.0 / 59.0	105.0 / 47.0
60	97.0 / 60.0	103.0 / 59.0	105.0 / 48.0
Average Meter Temperature, °F (Tm)	91.0 / --	100.4 / --	104.3 / --
Average Meter Temperature, °R (Tm)	551.0 / --	560.4 / --	564.3 / --
Barometric Pressure, in. Hg (Pb)	28.44	28.44	28.44
Meter Orifice Pressure, in. WC (ΔH)	1.000	1.000	1.000
Meter Pressure, in. Hg (Pm)	28.51	28.51	28.51
Standard Meter Volume, ft <sup>3</sup> (Vmstd)	34.230	34.162	33.955
Impinger 1, Pre/Post Test, mL	462.4 / 475.0	475.0 / 488.0	488.0 / 499.6
Impinger 2, Pre/Post Test, mL	453.0 / 456.8	456.8 / 459.6	459.6 / 462.5
Impinger 3, Pre/Post Test, mL	300.4 / 302.9	301.5 / 302.7	300.4 / 301.1
Impinger 4, Pre/Post Test, g	502.9 / 509.9	509.9 / 516.0	516.0 / 521.1
Volume Water Collected, mL (Vlc)	25.9	23.1	20.3
Standard Water Volume, ft <sup>3</sup> (Vwstd)	1.219	1.087	0.956
Moisture Fraction Measured (BWSmsd)	0.034	0.031	0.027
Moisture Fraction @ Saturation (BWSsat)	0.367	0.532	0.575
Moisture Fraction, unitless (BWS)	0.034	0.031	0.027
DGM Calibration Check Value (Yqa)	1.6	2.2	1.9

Location Becton-Dickinson Medical

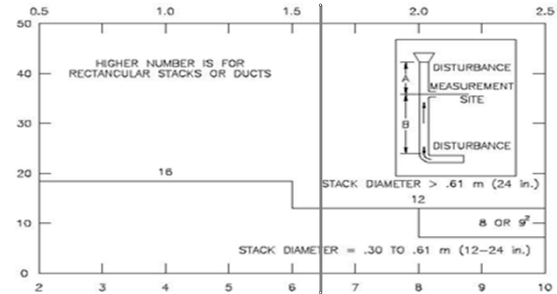
Source Catalytic Oxidizer - Inlet

Project No. 18-0668D

Date: 07/11/18

## Stack Parameters

Duct Orientation: Horizontal  
Duct Design: Circular  
Distance from Far Wall to Outside of Port: 27.50 in  
Nipple Length: 4.75 in  
Depth of Duct: 23.25 in  
Width of Duct: -- in  
Cross Sectional Area of Duct: 2.95 ft<sup>2</sup>  
Equivalent Diameter: -- in  
No. of Test Ports: 2  
Distance A: 5.4 ft  
Distance A Duct Diameters: 2.8 (must be > 0.5)  
Distance B: 12.5 ft  
Distance B Duct Diameters: 6.5 (must be > 2)  
Minimum Number of Traverse Points: 12  
Actual Number of Traverse Points: 16



## CIRCULAR DUCT

### LOCATION OF TRAVERSE POINTS

Number of traverse points on a diameter

	2	3	4	5	6	7	8	9	10	11	12
1	14.6	--	6.7	--	4.4	--	3.2	--	2.6	--	2.1
2	85.4	--	25.0	--	14.6	--	10.5	--	8.2	--	6.7
3	--	--	75.0	--	29.6	--	19.4	--	14.6	--	11.8
4	--	--	93.3	--	70.4	--	32.3	--	22.6	--	17.7
5	--	--	--	--	85.4	--	67.7	--	34.2	--	25.0
6	--	--	--	--	95.6	--	80.6	--	65.8	--	35.6
7	--	--	--	--	--	--	89.5	--	77.4	--	64.4
8	--	--	--	--	--	--	96.8	--	85.4	--	75.0
9	--	--	--	--	--	--	--	--	91.8	--	82.3
10	--	--	--	--	--	--	--	--	97.4	--	88.2
11	--	--	--	--	--	--	--	--	--	--	93.3
12	--	--	--	--	--	--	--	--	--	--	97.9

\*Percent of stack diameter from inside wall to traverse point.

Traverse Point	% of Diameter	Distance from inside wall	Distance from outside of port
1	3.2	0.74	5.49
2	10.5	2.44	7.19
3	19.4	4.51	9.26
4	32.3	7.51	12.26
5	67.7	15.74	20.49
6	80.6	18.74	23.49
7	89.5	20.81	25.56
8	96.8	22.51	27.26
9	--	--	--
10	--	--	--
11	--	--	--
12	--	--	--

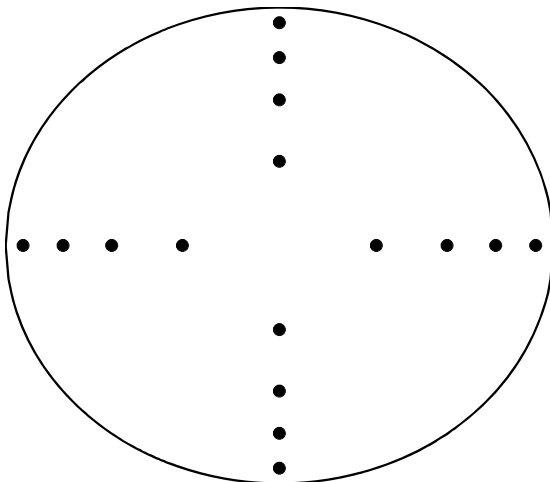
Stack Diagram

A = 5.42 ft.

B = 12.5 ft.

Depth of Duct = 23.25 in.

Cross Sectional Area



Downstream Disturbance

A

B

Upstream Disturbance

**Location** Becton-Dickinson Medical

**Source** Catalytic Oxidizer - Inlet

**Project No.** 18-0668D

**Date** 7/11/18

Sample Point	Angle ( $\Delta P=0$ )
1	3
2	4
3	7
4	6
5	9
6	11
7	12
8	14
9	5
10	6
11	5
12	7
13	8
14	4
15	6
16	5
Average	7.0



Location Becton-Dickinson Medical  
Source Catalytic Oxidizer - Inlet  
Project No. 18-0668D

Run No.	1		2		3	
Date	7/11/18		7/11/18		7/11/18	
Status	VALID		VALID		VALID	
Start Time	10:45		11:51		12:43	
Stop Time	10:56		11:59		12:51	
Leak Check	Pass		Pass		Pass	
Traverse Point	$\Delta P$ (in. WC)	Ts (°F)	$\Delta P$ (in. WC)	Ts (°F)	$\Delta P$ (in. WC)	Ts (°F)
A1	0.20	93	0.22	102	0.22	99
2	0.23	94	0.23	101	0.20	101
3	0.25	94	0.23	101	0.23	102
4	0.25	94	0.22	101	0.22	102
5	0.24	94	0.22	100	0.21	101
6	0.24	93	0.23	100	0.22	101
7	0.26	93	0.21	99	0.23	100
8	0.23	93	0.17	97	0.18	97
B1	0.21	93	0.20	100	0.21	99
2	0.24	93	0.22	100	0.23	100
3	0.26	93	0.24	100	0.24	100
4	0.24	93	0.23	100	0.22	101
5	0.25	93	0.23	101	0.24	101
6	0.24	94	0.24	103	0.23	102
7	0.25	94	0.22	102	0.22	102
8	0.22	94	0.22	102	0.23	102

Average					
Square Root of $\Delta P$ , (in. WC) <sup>1/2</sup>	( $\Delta P$ ) <sup>1/2</sup>	0.488	0.469	0.469	0.475
Average $\Delta P$ , in. WC	( $\Delta P$ )	0.24	0.22	0.22	0.23
Pitot Tube Coefficient	(Cp)	0.833	0.833	0.833	0.833
Barometric Pressure, in. Hg	(Pb)	28.44	28.44	28.44	28.44
Static Pressure, in. WC	(Pg)	-7.30	-7.00	-7.20	-7.17
Stack Pressure, in. Hg	(Ps)	27.90	27.93	27.91	27.91
Average Temperature, °F	(Ts)	93.4	100.6	100.6	98.2
Average Temperature, °R	(Ts)	553.4	560.6	560.6	558.2
Moisture Fraction	(BWS)	0.034	0.031	0.027	0.031
Molecular Weight, lb/lb-mole (dry)	(Md)	29.00	29.00	29.00	29.00
Molecular Weight, lb/lb-mole (wet)	(Ms)	28.62	28.66	28.70	28.66
Velocity, ft/sec	(Vs)	28.9	28.0	28.0	28.3
VFR at stack conditions, acfm	(Qa)	5,114	4,948	4,947	5,003
VFR at standard conditions, scfh	(Qsw)	273,019	261,009	260,793	264,940
VFR at standard conditions, scfm	(Qsw)	4,550	4,350	4,347	4,416
VFR at standard conditions, dscfm	(Qsd)	4,394	4,216	4,228	4,279

Sample Analysis (Inlet)												
Run 1												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.076	1291768.2	2.077	477331.4	2.077	1408321.9	2.078	2018887.9	2.079	2003382	2.078	1439938 656.68
Run 2												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.082	1935611.6	2.084	2062107.8	2.085	2523314	2.087	1567394.5	2.087	2041732.7	2.085	2026032 923.96
Run 3												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.09	2220462.5	2.088	2557967.3	2.092	1901202.1	2.091	3079176.5	2.091	2195096.5	2.090	2390781 1090.30

Sample Analysis (Outlet)												
Run 1												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.744	279.278	2.737	139.59	2.747	135.79	2.746	51.2	2.732	64.0	2.741	134 0.05
Run 2												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.734	53.43	2.764	74.7	2.738	91.9	2.727	57.82	2.733	132.5	2.739	82 0.03
Run 3												
Cpd	Inj. 1		Inj. 2		Inj. 3		Inj. 4		Inj. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC ppm
Ethylene Oxide	2.737	117.9	2.751	109.36	2.764	82.29	2.727	96.82	2.708	106.58	2.737	103 0.04

## Appendix C



## Wind Tunnel Pitot Calibration

S-type Pitot ID: **P-1103** Date: **3-Apr-17**  
 Standard Pitot ID: **001** Personnel: **DH**  
 Cp(std): **0.99** Cp(actual): **0.833**  
 Part Number: **PPS12-Y-007.5** P<sub>bar</sub>(in Hg): **29.61**  
 Test Velocity (fps): **50** T(°F): **71**

A-SIDE	$\Delta P_{std}$ (in. H <sub>2</sub> O)	$\Delta P_s$ (in. H <sub>2</sub> O)	Cp(s)	Deviation*
	0.547	0.767	0.836	-0.002
	0.548	0.759	0.841	0.003
	0.549	0.764	0.839	0.001
	0.545	0.766	0.835	-0.003
	<b>AVERAGE</b>		<b>0.838</b>	0.002
			Std deviation	0.003

B-SIDE	$\Delta P_{std}$ (in. H <sub>2</sub> O)	$\Delta P_s$ (in. H <sub>2</sub> O)	Cp(s)	Deviation*
	0.547	0.784	0.828	-0.001
	0.547	0.781	0.829	0.000
	0.548	0.782	0.829	0.000
	0.551	0.782	0.831	0.002
	<b>AVERAGE</b>		<b>0.829</b>	0.001
			Std deviation	0.001

$$Cp(s) = Cp(std) \sqrt{\frac{\Delta P(std)}{\Delta P(s)}}$$

$$Cp(A) - Cp(B) = \boxed{0.009} \text{ \{must be <0.010\}}$$

$$*Deviation = \{Cp(s) - AVG Cp(s)\} \text{ \{must be <0.010\}}$$

Standard deviation of the deviations must be less than 0.02 for both sides.

Pitot tube S/N P-1103 was calibrated in accordance with the CFR 40, Part 60 Appendix A, Method 2, Section 10.

  
Signature

  
Date

# METHOD 5 DRY GAS METER CALIBRATION USING CRITICAL ORIFICES

- 1) Select three critical orifices to calibrate the dry gas meter which bracket the expected operating range.
- 2) Record barometric pressure before and after calibration procedure.
- 3) Run at tested vacuum (from Orifice Calibration Report), for a period of time necessary to achieve a minimum volume of 10 cubic feet Vcr (STD). K' factors of ~8025 = 13 minutes, .5011 = 20 minutes, .3433 = 30 minutes
- 4) Record data and information in the **GREEN** cells, **YELLOW** cells are calculated.

DATE: 6/27/2018		DGM SERIAL NUMBER: 18654628		BAROMETRIC PRESSURE (mbar): INITIAL 837 FINAL 837		AVG (P <sub>amb</sub> ) 837	
METER PART #: NA		CRITICAL ORIFICE MFG: Apex		BAROMETRIC PRESSURE (in Hg): INITIAL 24.71661 FINAL 24.71661		AVG (P <sub>amb</sub> ) 24.71661	
METHOD 5 BOX ID: M5-10							
TECHNICIAN/OPERATOR: Phil Brock							

ORIFICE #	RUN #	K' FACTOR (AVG)	TESTED VACUUM (in Hg)	DGM READINGS (FT <sup>3</sup> )		TEMPERATURES °F				ELAPSED TIME (MIN)	DGM ΔH (in H <sub>2</sub> O)	(1) V <sub>cr</sub> (STD)	(2) V <sub>cr</sub> (STD)	(3) Y	ΔH <sub>g</sub>		
				INITIAL	FINAL	NET (V <sub>cr</sub> )	AMBIENT	DGM INLET	DGM OUTLET							DGM	
48	1	0.3433	20.0	450.0	460.508	10.508	76	77	78	76	77	77	8.5480	8.7987	1.029	1.53	
	2	0.3433	20.0	460.508	471.046	10.538	77	78	78	77	78	77.75	8.5605	8.7905	1.027	1.53	
	3	0.3433	20.0	471.046	481.610	10.564	77	78	76	78	76	77	8.5936	8.7905	1.023	1.53	
63	1	0.5849	17.5	418.001	428.483	10.482	75	74	75	72	74	73.75	8.6030	8.7528	1.017	1.65	
	2	0.5849	17.5	428.483	438.956	10.473	76	75	76	74	75	75	8.5755	8.7446	1.020	1.65	
	3	0.5849	17.5	438.956	449.467	10.511	76	76	77	75	75	75.75	8.5946	8.7446	1.017	1.65	
73	1	0.8025	15.5	482.004	493.450	11.446	76	75	75	75	75	75	9.4084	9.4269	1.002	1.70	
	2	0.8025	15.5	493.450	504.817	11.367	75	75	76	75	75	76.25	9.3390	9.4357	1.010	1.70	
	3	0.8025	15.5	504.817	516.157	11.340	76	76	78	75	76	76.25	9.2995	9.4269	1.014	1.70	
												AVG = 1.018		AVG = 1.009			

USING THE CRITICAL ORIFICES AS CALIBRATION STANDARDS:  
The following equations are used to calculate the standard volumes of air passed through the DGM, V<sub>cr</sub> (std), and the critical orifice, V<sub>c</sub> (std), and the DGM calibration factor, Y. These equations are automatically calculated in the spreadsheet above.

AVERAGE DRY GAS METER CALIBRATION FACTOR, Y = 1.018

AVERAGE ΔH<sub>g</sub> = 1.63

$$(1) \quad V_{m_{(std)}} = K_1 * V_m * \frac{P_{bar} + (\Delta H / 13.6)}{T_m}$$

= Net volume of gas sample passed through DGM, corrected to standard conditions  
K<sub>1</sub> = 17.64 °R/in. Hg (English), 0.3858 °K/mm Hg (Metric)  
T<sub>m</sub> = Absolute DGM avg. temperature (°R - English, °K - Metric)

$$(2) \quad V_{cr_{(std)}} = K' * \frac{P_{bar} * \Theta}{\sqrt{T_{amb}}}$$

= Volume of gas sample passed through the critical orifice, corrected to standard conditions  
T<sub>amb</sub> = Absolute ambient temperature (°R - English, °K - Metric)

$$(3) \quad Y = \frac{V_{cr_{(std)}}}{V_{m_{(std)}}}$$

= DGM calibration factor  
K' = Average K' factor from Critical Orifice Calibration

$$\Delta H_g = \left( \frac{0.758}{V_{cr(std)}} \right)^2 \Delta H \left( \frac{V_{m(std)}}{V_m} \right)$$

## Pyrometer Calibration Data

Calibration Temp. Reading (F)	Pyrometer Reading (F)	ABS (Relative Difference) % R
0	1	0.2
50	49	0.2
100	99	0.2
150	149	0.2
250	251	0.1
500	499	0.1
800	802	0.2
Max Absolute Difference %		0.2

Omega Temp Calibrator ID 1  
Omega Temp Calibrator S/N... T-197197  
Calibration Date..... 7/27/2017  
Recent Date..... 7/27/2018

# CERTIFICATE OF ANALYSIS

## Grade of Product: CERTIFIED STANDARD-SPEC

Customer:	AIR LIQUIDE POLLUTION INC	Reference Number:	126-400855163-1
Part Number:	X02NI99C15A5263	Cylinder Volume:	144.4 CF
Cylinder Number:	ALM-014712	Cylinder Pressure:	2015 PSIG
Laboratory:	124 - La Porte Mix - TX	Valve Outlet:	350
Analysis Date:	Feb 15, 2017		
Lot Number:	126-400855163-1		

**Expiration Date: Feb 15, 2019**

Product composition verified by direct comparison to calibration standards traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

## ANALYTICAL RESULTS

Component	Req Conc	Actual Concentration (Mole %)	Analytical Uncertainty
ETHYLENE OXIDE	50.00 PPM	50.02 PPM	+/- 2%
NITROGEN	Balance		

### Notes:

AIR LIQUIDE POLLUTION INC  
PO#: D00FC  
PO#: 4510145652



Signature on file

Approved for Release

# CERTIFICATE OF ANALYSIS

## Grade of Product: CERTIFIED STANDARD-SPEC

Customer:	AIR LIQUIDE POLLUTION INC	Reference Number:	126-400855162-1
Part Number:	X02NI99C15A0631	Cylinder Volume:	144.9 CF
Cylinder Number:	ALM013685	Cylinder Pressure:	2015 PSIG
Laboratory:	124 - La Porte Mix - TX	Valve Outlet:	350
Analysis Date:	Feb 15, 2017		
Lot Number:	126-400855162-1		

**Expiration Date: Feb 15, 2019**

Product composition verified by direct comparison to calibration standards traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

## ANALYTICAL RESULTS

Component	Req Conc	Actual Concentration (Mole %)	Analytical Uncertainty
ETHYLENE OXIDE	5210 PPM	5222 PPM	+/- 2%
NITROGEN	Balance		

### Notes:

AIR LIQUIDE POLLUTION INC  
PO#: D0OFC  
PO#: 4510145652



Signature on file

Approved for Release

**Location** Becton-Dickinson Medical

**Source** Catalytic Oxidizer - Outlet

**Project No.** 18-0668D

**Parameter** VFR

<b>Date</b>	<b>Pitot ID</b>	<b>Evidence of damage?</b>	<b>Evidence of mis-alignment?</b>	<b>Calibration or Repair required?</b>
7/11/18	P-1103	no	no	no
<b>Date</b>	<b>Barometric Pressure</b>	<b>Evidence of damage?</b>	<b>Reading Verified</b>	<b>Calibration or Repair required?</b>
7/11/18	Weather Station	NA	NA	NA



## Becton-Dickinson Medical

## Catalytic Oxidizer

7/10/2018

## EPA Method 18: Determination of Gaseous Organic Compounds using Gas Chromatography

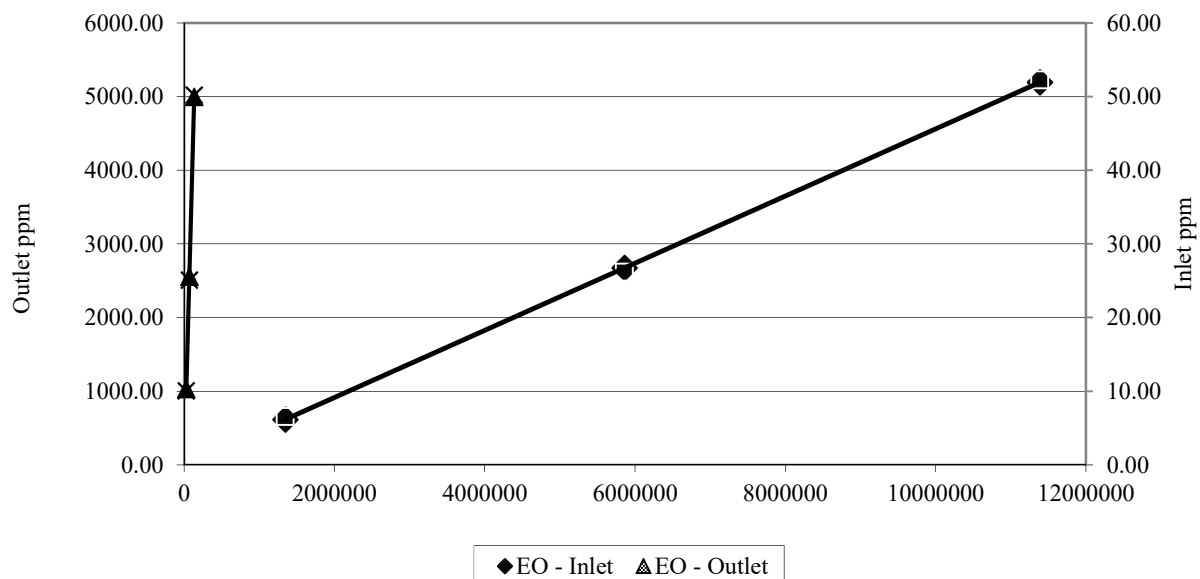
Initial Three-Point Calibration									
(Inlet) High Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1		Inj. 2		Inj. 3		Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	5222.00	2.055	11592055.0	2.056	11610124.0	2.058	10970216.0	2.056	11390798
Mid-Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1		Inj. 2		Inj. 3		Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	2611.00	2.059	5862940.0	2.06	5875961.5	2.061	5843135.0	2.060	5860679
Low-Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1	Sig.20015	Inj. 2	Sig.20016	Inj. 3	Sig.20017	Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	652.75	2.063	1360158.6	2.063	1357636.1	2.065	1327310.4	2.064	1348368

Initial Three-Point Calibration									
(Outlet) Low Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1		Inj. 2		Inj. 3		Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	50.20	2.835	137098.9	2.834	134495	2.833	134893.3	2.834	135496
Mid-Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1		Inj. 2		Inj. 3		Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	25.10	2.831	69592.3	2.828	69026.3	2.828	69224.8	2.829	69281
Low-Level Calibration Standard									
Cpd ID	Conc. (ppm)	Inj. 1		Inj. 2		Inj. 3		Average	
		RT	AC	RT	AC	RT	AC	RT	AC
Ethylene Oxide	10.04	2.823	27865.7	2.82	28054.3	2.817	27607.4	2.820	27842

## Linear Regression Calculations

EO - Inlet			
Certified ppm	Average AC	Linear Regression Statistics	ppm from curve
5222.00	11390798	$R^2$ $M$	5194.72
2611.00	5860679	0.9994    0.00045604	2672.73
652.75	1348368		614.92

EO - Outlet			
Certified ppm	Average AC	Linear Regression Statistics	ppm from curve
50.20	135496	$R^2$ $M$	49.93
25.10	69281	0.9999    0.00036853	25.53
10.04	27842		10.26



Becton-Dickinson Medical

Catalytic Oxidizer

7/10-11/2018

EPA Method 18: Determination of Gaseous Organic Compounds using Gas Chromatography

Quality Assurance Inlet												
Inlet Line Loss Check (High-level calibration gas to the sample probe)												
Cpd ID	Conc. (ppm)	Inj. 1 RT	Sig. 10059 AC	Inj. 2 RT	Sig. 10060 AC	Inj. 3 RT	Sig.10061 AC	Average RT	AC	ppm	Triplicate OK?	Recovery OK?
Ethylene Oxide	5222.00	2.074	10710042	2.072	10817854	2.072	10788828	2.073	10772241	4912.63	Y	Y

Inlet Post Test Calibration Check (mid-level calibration gas to the gas sampling valve)												
Cpd ID	Conc. (ppm)	Inj. 1 RT	AC	Inj. 2 RT	AC	Inj. 3 RT	AC	Average RT	AC	ppm	Triplicate OK?	Pre/Post OK?
Ethylene Oxide	2611.00	2.096	5525176.0	2.098	5464539.0	2.092	5833090.5	2.095	5607602	2557.32	Y	Y

Run #2 Unspiked Bag Inlet												
Cpd ID	Conc. (ppm)	Inj. 1 RT	AC	Inj. 2 RT	AC	Inj. 3 RT	AC	Average RT	AC	ppm	Triplicate OK?	Recovery OK?
Ethylene Oxide	Unkown	2.082	2153093.3	2.081	2103305.2	2.081	2158600	2.081	2138333	975.18	Y	

Post Test Spike Check (50:50 high-level calibration gas and Run #2)												
Cpd ID	Target Conc. (ppm)	Inj. 1 RT	AC	Inj. 2 RT	AC	Inj. 3 RT	AC	RT	Average AC	ppm	Triplicate OK?	Spike OK?
Ethylene Oxide	3098.59	2.078	6369979.5	2.078	6313084	2.078	6307601.5	2.078	6330222	2886.87	Y	Y

Becton-Dickinson Medical

Catalytic Oxidizer

7/10-11/2018

EPA Method 18: Determination of Gaseous Organic Compounds using Gas Chromatography

Quality Assurance Outlet												
Outlet Line Loss Check (High-level calibration gas to the sample probe)												
Cpd ID	Conc. (ppm)	Inj. 1 RT	Sig.20059 AC	Inj. 2 RT	Sig. 20060 AC	Inj. 3 RT	Sig.20061 AC	Average RT	AC	ppm	Triplicate OK?	Recovery OK?
Ethylene Oxide	50.20	2.738	126166.6	2.746	126469.3	2.744	124657.2	2.743	125764	46.35	Y	Y

Outlet Post Test Calibration Check (mid-level calibration gas to the gas sampling valve)												
Cpd ID	Conc. (ppm)	Inj. 1 RT	Sig.10043 AC	Inj. 2 RT	Sig.10044 AC	Inj. 3 RT	Sig.10045 AC	Average RT	AC	ppm	Triplicate OK?	Pre/Post OK?
Ethylene Oxide	25.10	2.695	64944.3	2.696	65305.8	2.698	67455.6	2.696	65902	24.29	Y	Y

Run #2 Unspiked Bag Outlet												
Cpd ID	Conc. (ppm)	Inj. 1 RT	AC	Inj. 2 RT	AC	Inj. 3 RT	AC	Average RT	AC	ppm	Triplicate OK?	Recovery OK?
Ethylene Oxide	Unkown	2.780	75.1	2.78	10.2	2.780	165.9	2.780	84	0.03		

Post Test Spike Check (50:50 high-level calibration gas and Run #2)												
Cpd ID	Target Conc. (ppm)	Inj. 1 RT	AC	Inj. 2 RT	AC	Inj. 3 RT	AC	RT	Average AC	ppm	Triplicate OK?	Spike OK?
Ethylene Oxide	25.12	2.780	63384.6	2.78	63893.9	2.779	63522.2	2.780	63600	23.44	Y	Y

## Appendix D

# Lesni Stack Pre-Test Data

Date: 11 Jul 18

Recorded By: Daniel T Gaunt

Post Valve  
Ch 2

Post Valve  
Ch 2

Post Valve  
Ch 3

Time	% LEL 30.630	% LEL 30.633	Inlet Bed Temp °C (Control) 25.610	Outlet Bed Temp °C 25.611
940	0.0	0.0	161	160
9:50 AM	0.0	0.0	160	161
10:00 AM	1.20	2.0	160	160
10:10 AM	0.0	0.8	160	160
10:20 AM	1.8	2.3	160	163
10:30 AM	1.8	3.1	159	168
10:40 AM	2.7	3.8	160	172
10:50 AM	2.6	3.3	159	179
11:00 AM	0.0	0.5	161	183
11:10 AM	2.2	3.2	160	186
11:20 AM	2.6	3.2	160	184
11:30 AM	1.2	1.9	160	182
11:40 AM	2.6	3.2	160	186
11:50 AM	2.7	3.3	159	187
12:00 PM	1.8	2.6	161	185
12:10 PM	3.2	3.8	159	188
12:20 PM	3.1	3.9	161	188
12:30 PM	2.8	3.3	160	188
12:40 PM	2.6	3.3	159	189
12:50 PM	3.5	4.3	161	192
1:00 PM	<del>5.3</del> 3.3	6.0	161	193
1:10 PM	6.3	5.8	160	194
1:20 PM	2.7	3.7	161	198
1:30 PM	2.9	3.8	162	198
1:40 PM	3.7	4.7	163	200

## Lesni Stack Pre-Test Data

Date: 11 Jul 18

Recorded By: Daniel T Gaunt

[illegible]

**Last Page of Report**